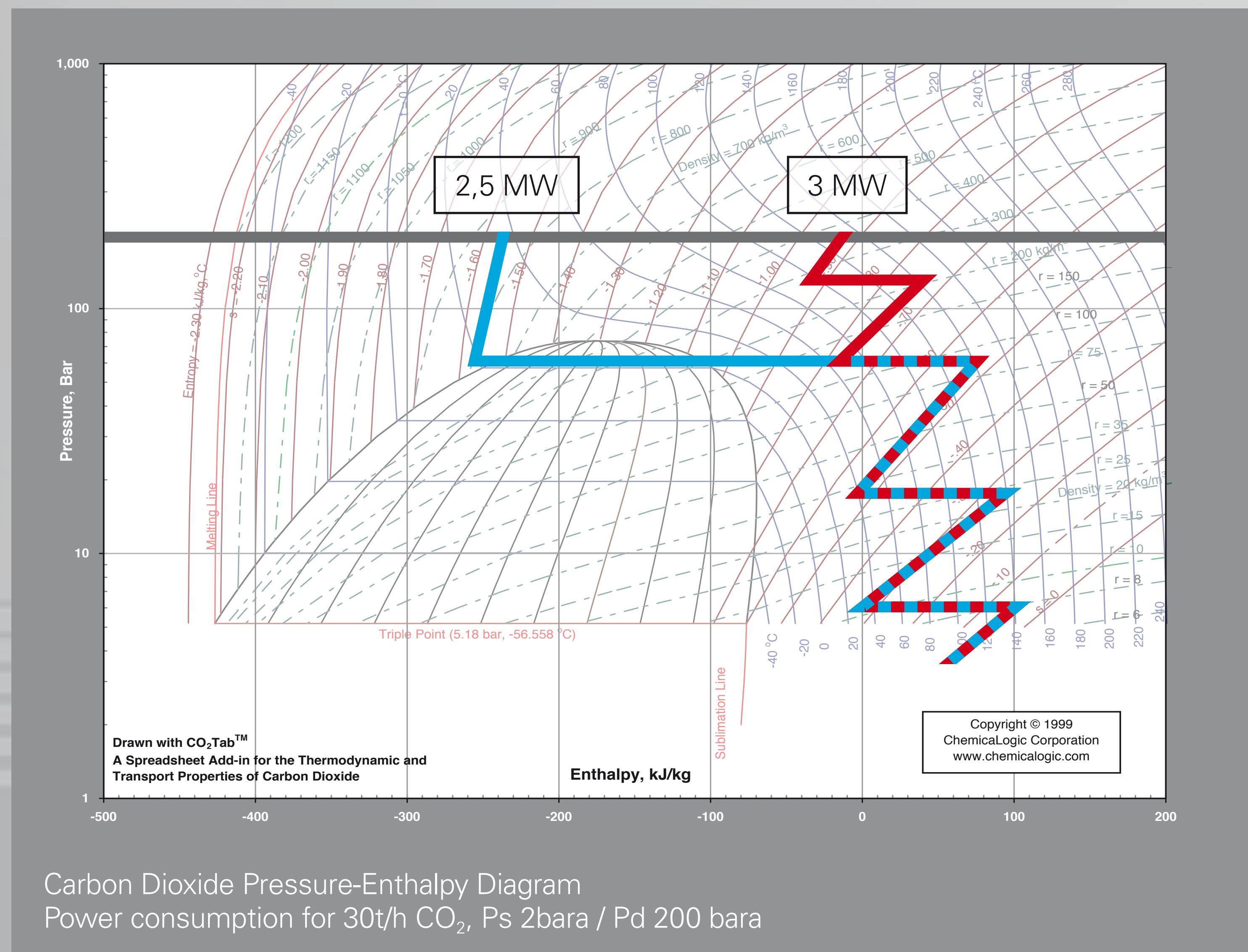


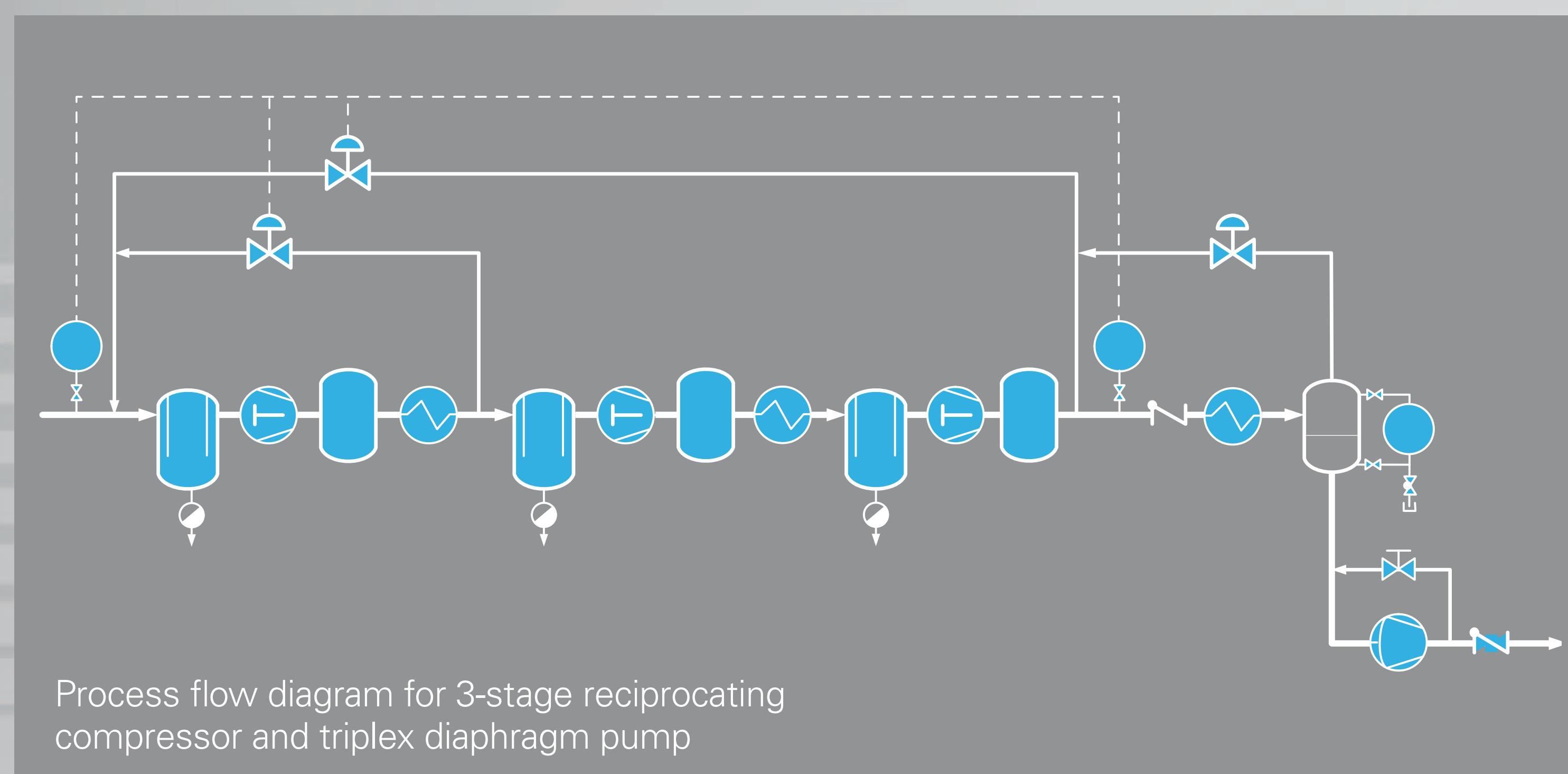
Improving efficiency of CO₂ compression for CCS and EOR with reciprocating compressors and diaphragm pumps

Case study for 30 t/h CO₂ vs. 200 bar

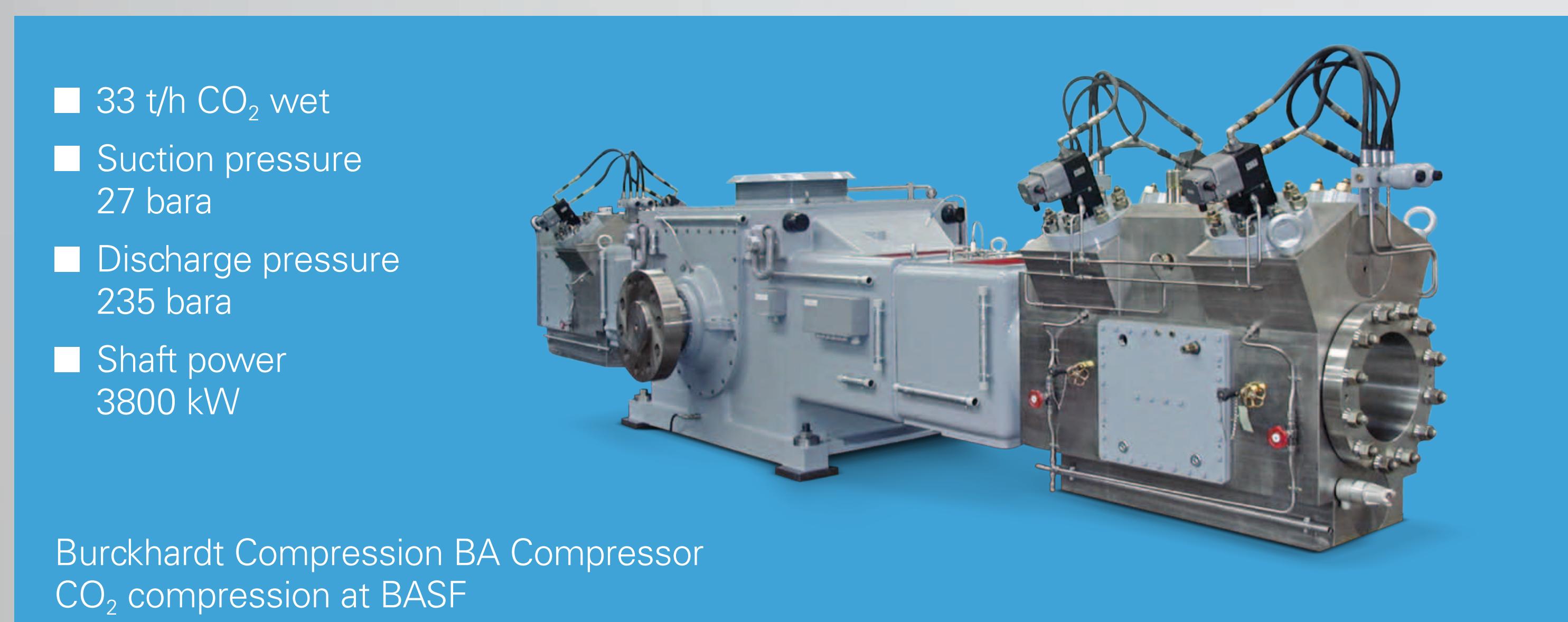
Rainer Dübi, Dr. Luzi Valär, Burckhardt Compression, Im Link 5, 8404 Winterthur, Switzerland
 Dr. Josef Jarosch, Anke Braun, LEWA GmbH, Ulmer Straße 10, 71229 Leonberg, Germany



Carbon Dioxide Pressure-Enthalpy Diagram
 Power consumption for 30t/h CO₂, Ps 2bara / Pd 200 bara



Process flow diagram for 3-stage reciprocating compressor and triplex diaphragm pump



Burckhardt Compression BA Compressor
 CO₂ compression at BASF



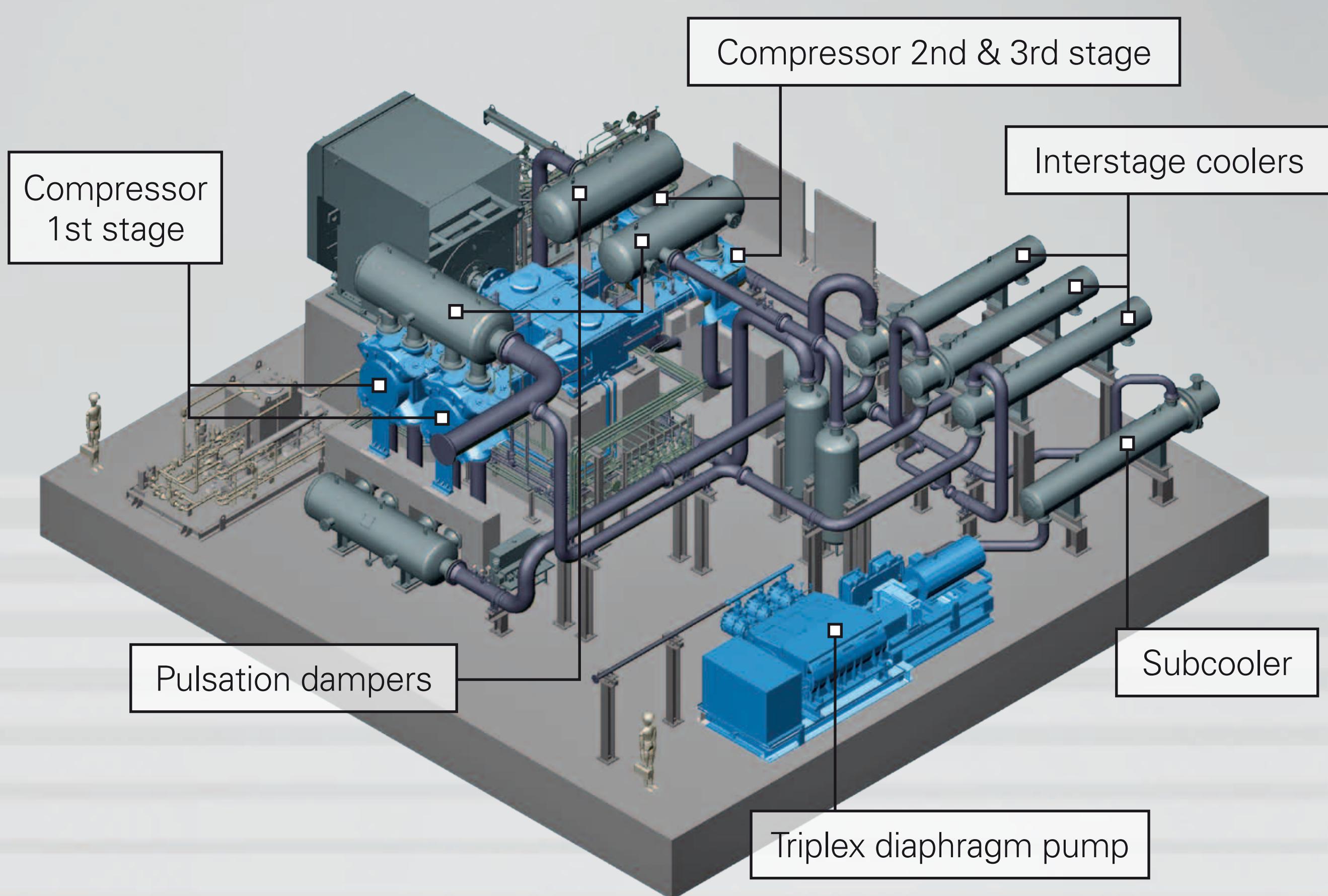
LEWA Diaphragm Pump G4T
 CCS at Snøhvit Gas Field

- Conventional way of compression

- 5 compressor stages
- Corrosion due to decompression in packing and sealing elements (stage 4 + 5)
- Increase on electrical power demand and stages due to high suction temperature
- 3 MW shaft power

+ Combined way of compression

- 3 compressor stages + triplex diaphragm pump
- Subcooling to liquid phase
- 2,5 MW shaft power



Plant layout for compressing 30t/h CO₂

Advantages

- Electrical power saving ~15%
- Flexible operation
 - Part load
 - Energy efficiency in part load
 - Gas composition
 - Discharge pressure
- Combined solution offered in cooperation by Burckhardt Compression and LEWA

Limitations

- Mass flow ≤ 150 t/h
- Suction pressure: ≥ ambient pressure
- Discharge pressure: ≤ 500 bar
- Cooling requirement depending on mixture (~25°C pure CO₂)